

TERMINOLOGY

- **Pressure Drop** – The difference in upstream and downstream pressures of the fluid flowing through the valve.
- **Critical Flow** – The flow has reached the point of being choked. At the choked condition the flow rate has hit a maximum limit and does not increase with further increase in pressure drop across the valve.
- **Cv or Valve Flow Coefficient** – The number of U. S. gallons per minute of water at 60°F that will pass through the valve with a pressure drop of 1 psi. For example, a Hi-Flow™ valve with a maximum Cv of 10.75 has an effective port area in the full open position such that it passes 10.75 GPM of water with a pressure drop of 1 psi.
- **Full Port** – The port diameter of the valve is the same diameter as the piping connections.
- **Rangeability** – The ratio of maximum controllable flow to minimum controllable flow of a valve. For example, a valve with a 50 to 1 rangeability and a total flow capacity of 100 GPM at full open controls flow accurately to as low as 2 GPM.
- **Valve Flow Characteristic** – The relationship between the stem travel or rotation of a valve, expressed in percent travel, and the fluid flow through the valve, expressed in percent of full flow.

CONTROL VALVE SIZING



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The Cv method is an accepted way to size control valves. Basic equations are provided as a guide to use in sizing a control valve, and the results of the equations will only be as accurate as the information provided of the flowing conditions. The equations are broken down into the type of media - liquid, gas or steam, and whether or not the flow is critical. The critical flow equations are to be used for vapor flow when the pressure drop across the valve is greater than half of the upstream pressure. As a general guide to avoid cavitation do not size a valve for liquid service where the pressure drop is greater than 50% of the upstream pressure.

CONTROL VALVE ACTUATOR SIZING



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CONTROL VALVE FLOW



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NOMENCLATURE

- Cv = Valve flow coefficient
- g = Specific gravity of liquid at flowing conditions
- G = Specific gravity of gas at flowing conditions
- P1 = Upstream pressure, psia
- P2 = Downstream pressure, psia
- ΔP = Actual pressure drop (P1-P2), psi
- q = Liquid volumetric flow rate, U.S. GPM
- Q = Gas volumetric flow rate, SCFH
- W = Steam weight (mass) flow rate, LB/HR
- T = Flowing Temperature, °R (460 + °F)

Once the required Cv is determined, selection of the proper size control valve can be obtained by comparing the required Cv to the Cv values for the valve. As a general rule the maximum capacity of a control valve should be 15 to 50% above the maximum process flow, and the minimum required Cv must be within the available rangeability of the valve for proper control. If only the maximum process flow rate was used to calculate Cv, then the percent travel of the valve should be checked and should fall in the range of 65 to 80% of total travel.

SUB-CRITICAL FLOW

$$\text{Liquid } C_v = q \left(\frac{g}{\Delta P} \right)^{1/2}$$

$$\text{Gas } C_v = \frac{Q}{963} \left(\frac{G \times T}{\Delta P (P_1 + P_2)} \right)^{1/2}$$

$$\text{Steam } C_v = \frac{W}{2.1 [\Delta P (P_1 + P_2)]^{1/2}}$$

CRITICAL FLOW

$$\text{Gas or steam where } \Delta P > \frac{P_1}{2}$$

$$C_v = \frac{Q (G \times T)^{1/2}}{750 \times P_1}$$

$$C_v = \frac{W}{1.65 \times P_1}$$